

EUROPEAN HEAT PUMP SUMMIT

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Review on High Temperature Heat Pumps

Market Overview and Research Status

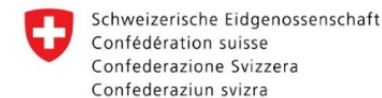
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In cooperation with the CTI



Swiss Confederation

Commission for Technology and Innovation CTI



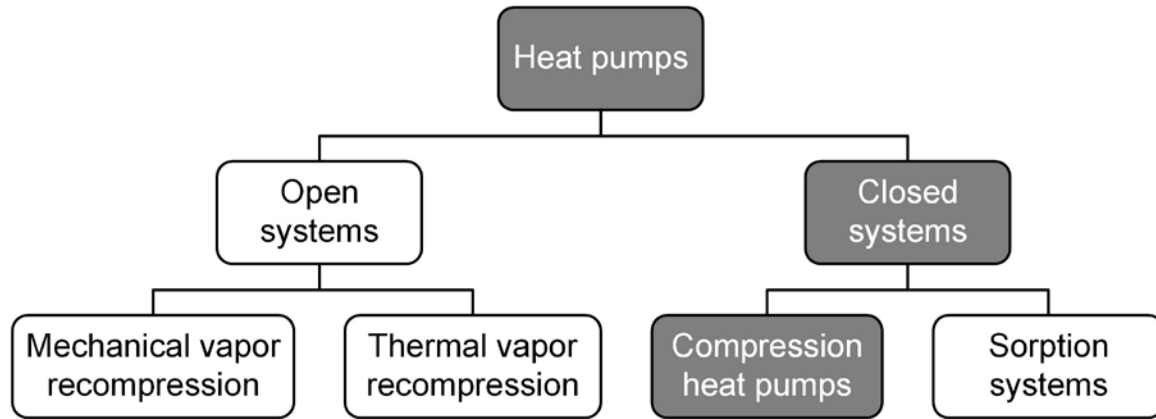
Outline

- 1. Market overview of commercially available industrial HTHP systems**
 - Cycles, refrigerants, application limits, efficiencies
- 2. Research status**
 - Screening of research activity
 - Experimental and theoretical studies, cycles, refrigerants, supply temperatures, operating ranges
- 3. Refrigerants**
 - Selection criteria, properties, GWP, price, efficiency, safety
- 4. Conclusions**

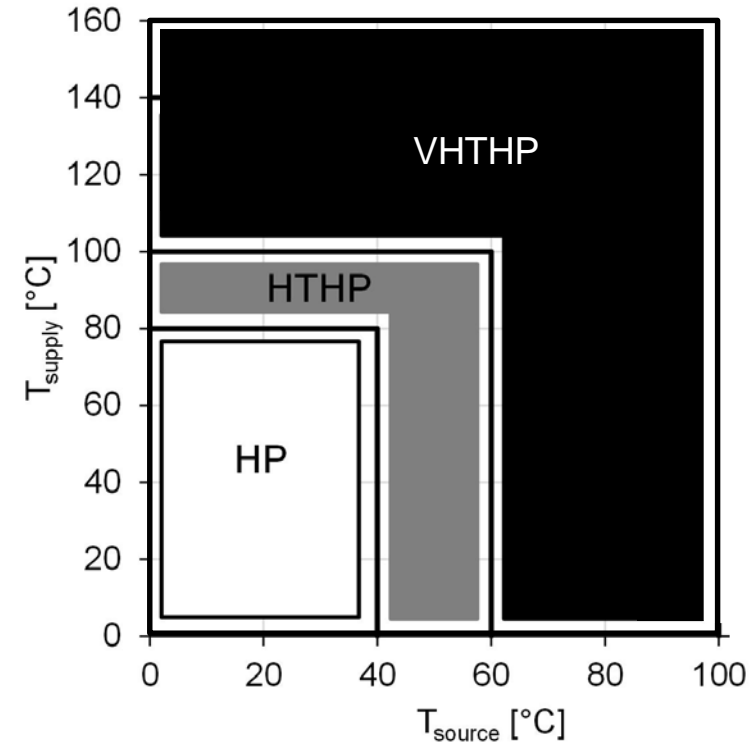


Classification of heat pumps (focus on compression heat pumps)

Development of temperature levels



adapted from Nellissen and Wolf (2015)



VHTHP: very high temperature heat pump

HTHP: high temperature heat pump

HP: conventional heat pump

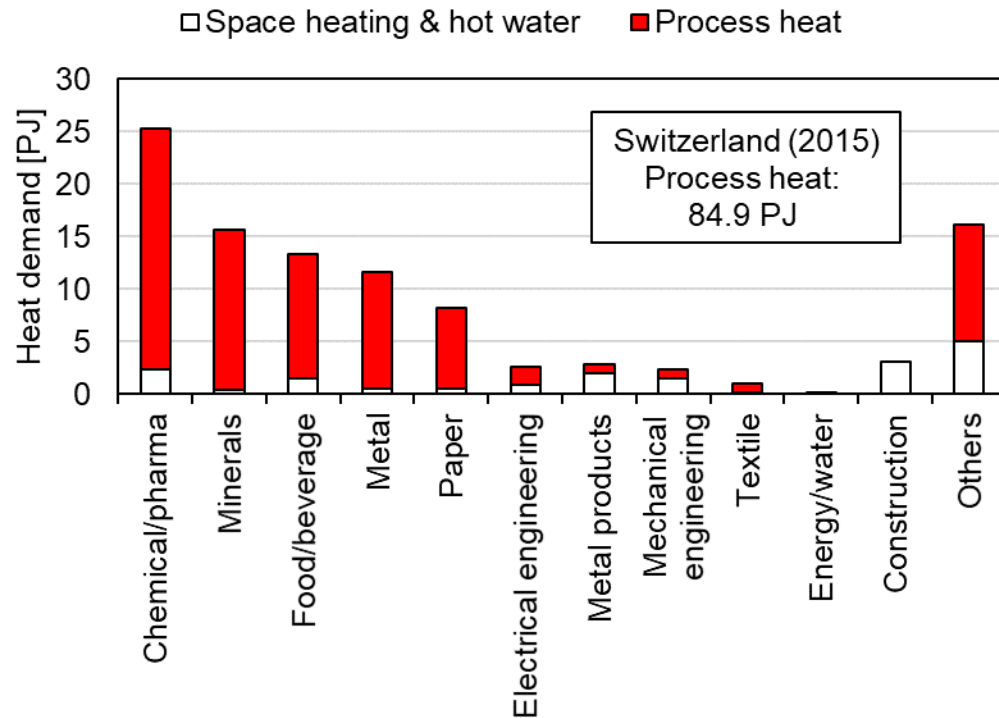
adapted from

Bobelin et al. (2012), IEA (2014), Jakobs and Laue (2015), Peureux et al. (2012, 2014)

Potential for high temperature heat pumps

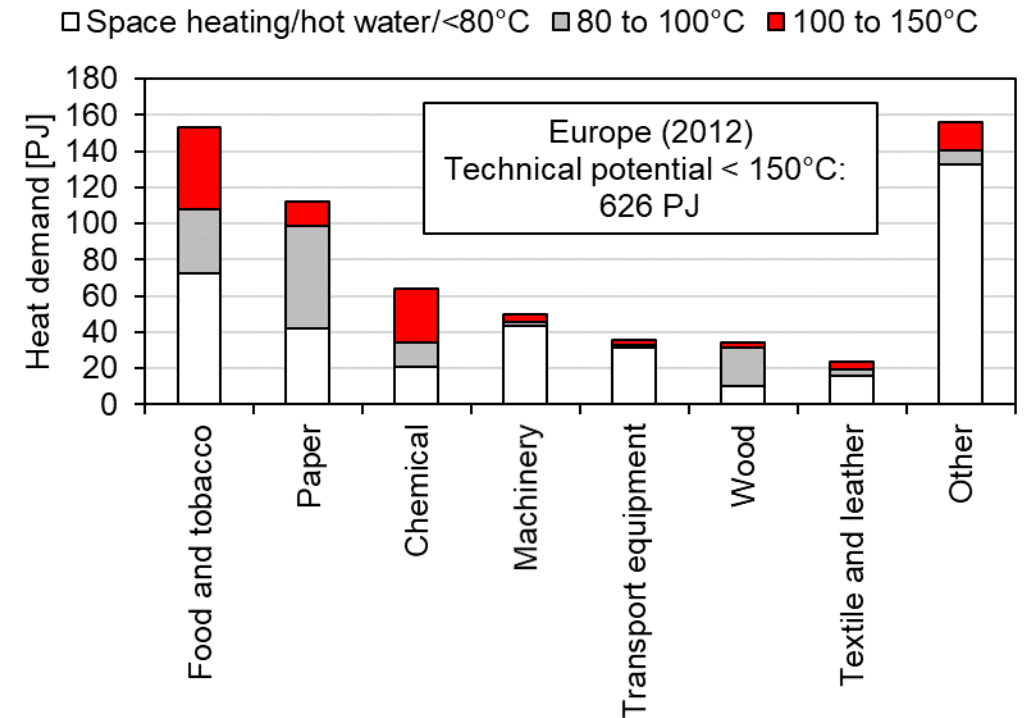
Process heat in industry

Theoretical potential for HTHPs in Switzerland



Data from BFE (2016), Pulfer and Spirig (2015)

Technical potential of process heat in Europe accessible with industrial heat pumps

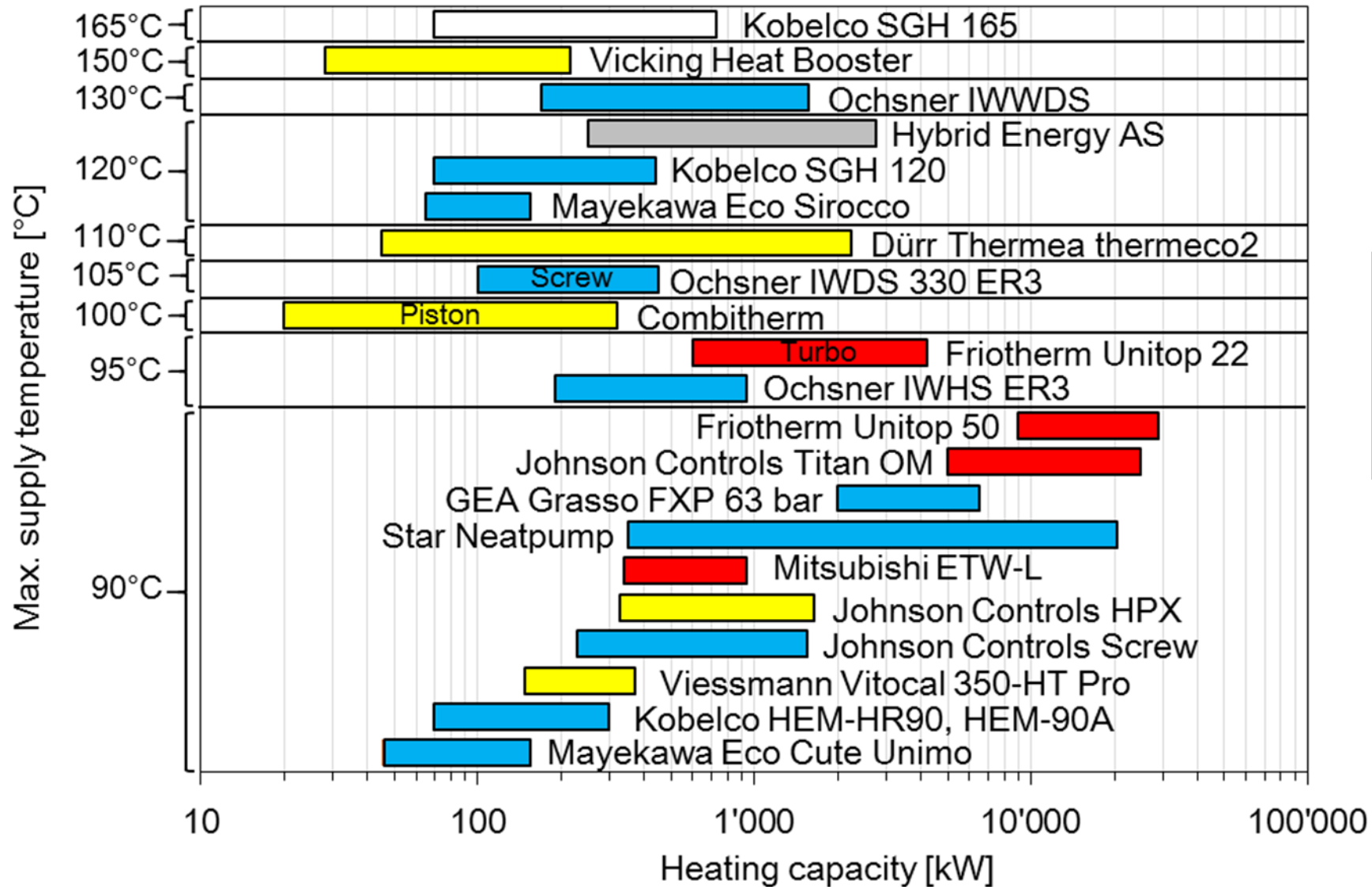


Based on Eurostat data from 2012 of 33 countries, Nellissen and Wolf (2015)

Selection of industrial HTHPs with supply temperatures > 90°C

Manufacturer	Product	Refrigerant	Max. supply temperature	Heating capacity	Compressor type	Reference
Kobe Steel (Kobelco Steam Grow Heat Pump)	SGH 165	R134a/R245fa	165°C	70 – 660 kW	Double screw	(IEA, 2014a; Kaida et al., 2015; Kuromaki, 2012; Watanabe, 2013)
	SGH 120	R245fa	120°C	70 – 370 kW		
	HEM-HR90,-90A	R134a/R245fa	90°C	70 – 230 kW		
Vicking Heating Engines AS	HeatBooster S4	R1336mzz(Z) R245fa	150°C	28 – 188 kW	Piston	(Nilsson, 2017; Nilsson et al., 2017; Viking Heat Engines AS, 2017)
Ochsner	IWWDS R2R3b	R134a/ÖKO1	130°C	170 – 750 kW	Screw (twin unit 1.5 MW)	(Ochsner, 2017a, 2017b, 2015; Zauner, 2016)
	IWWDS ER3b	ÖKO (R245fa)	130°C	170 – 750 kW		
	IWWHS ER3b	ÖKO (R245fa)	95°C	60 – 850 kW		
Hybrid Energy	Hybrid Heat Pump	R717 (NH ₃)	120°C	0.25 – 2.5 MW	Piston	(Hybrid Energy SA, 2017; Jensen et al., 2015a, 2015b)
Mayekawa	Eco Sirocco	R744 (CO ₂)	120°C	65 – 90 kW	Screw	(IEA, 2014a; Mayekawa, 2010; Watanabe, 2013)
	Eco Cute Unimo	R744 (CO ₂)	90°C	45 – 110 kW		
Dürr Thermea	thermeco ₂	R744 (CO ₂)	110°C	45 – 2'200 kW	Piston (up to 8 in parallel)	(Dürr thermea GmbH, 2017; IEA, 2014a; Thermea, 2012)
Combitherm	Customized design	R245fa	100°C	20 – 300 kW	Piston	(Blesl et al., 2014; Wolf et al., 2014)
Friotherm	Unitop 22	R1234ze(E)	95°C	0.6 – 3.6 MW	Turbo (two-stage)	(Friotherm AG, 2005; Wojtan, 2016)
	Unitop 50	R134a	90°C	9 – 20 MW		
Star Refrigeration	Neatpump	R717 (NH ₃)	90°C	0.35 – 15 MW	Screw (Vilter VSSH 76 bar)	(EMERSON, 2012)
GEA Refrigeration	GEA Grasso FX P 63 bar	R717 (NH ₃)	90°C	2 – 4.5 MW	Double screw (63 bar)	(Dietrich and Fredrich, 2012)
Johnson Controls	HeatPAC HPX	R717 (NH ₃)	90°C	326 – 1'324 kW	Piston (60 bar)	(Johnson Controls, 2017)
	HeatPAC Screw	R717 (NH ₃)	90°C	230 – 1'315 kW	Screw	
	Titan OM	R134a	90°C	5 – 20 MW	Turbo	
Mitsubishi	ETW-L	R134a	90°C	340 – 600 kW	Turbo (two-stage)	(IEA, 2014a; Watanabe, 2013)
Viessmann	Vitocal 350-HT Pro	R1234ze(E)	90°C	148 – 390 kW	Piston (2-3 in parallel)	(Viessmann, 2016)


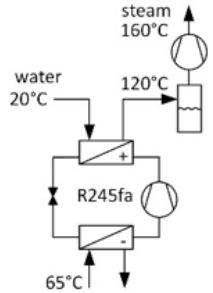

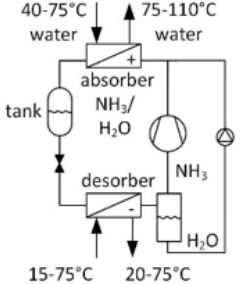

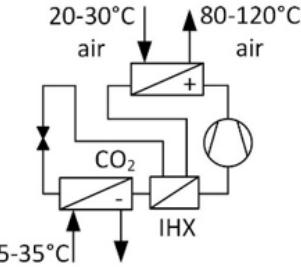

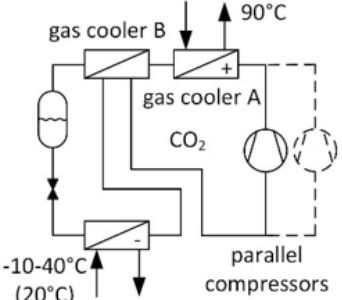

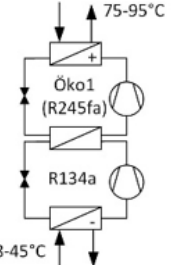

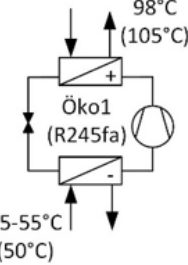
Commercially available industrial HTHPs sorted by maximum supply temperature and heating capacity




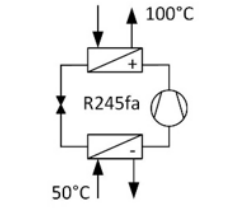

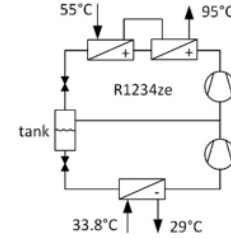

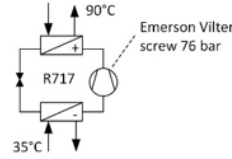
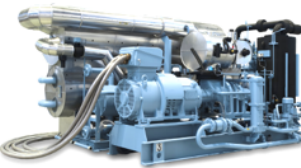
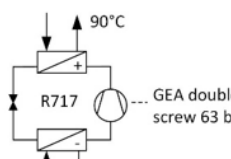

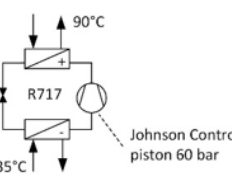

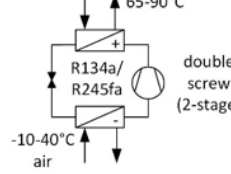

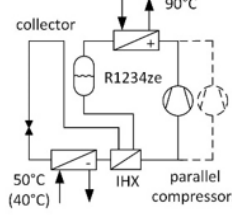

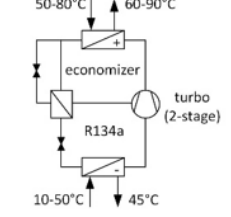
Compressor types:

- Screw
- Turbo
- Piston

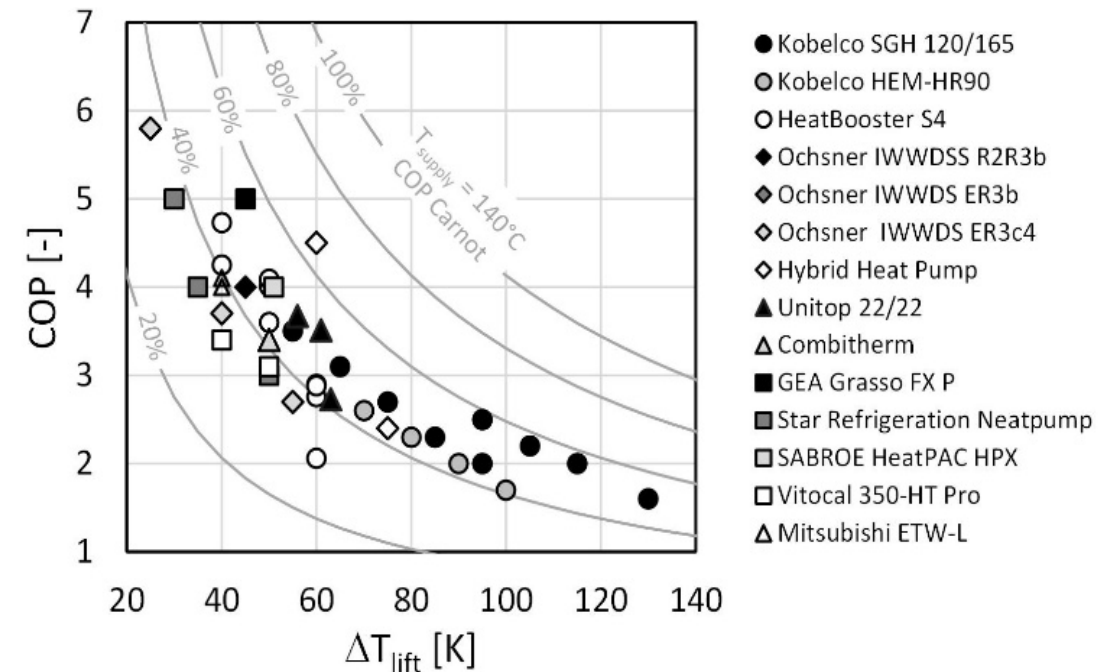
Commercial HTHPs – cycles, COPs and pictures

<p>Kobelco SGH 120 / 165</p>  <p>(IEA, 2014a; Kaida et al., 2015; Kuromaki, 2012; Watanabe, 2013)</p>	 <table border="1" data-bbox="762 525 1058 586"> <thead> <tr> <th>T_{LT}/T_{HT} (ΔT_{Lift})</th> <th>COP</th> </tr> </thead> <tbody> <tr> <td>65/120 (55)</td> <td>3.5</td> </tr> </tbody> </table>	T_{LT}/T_{HT} (ΔT_{Lift})	COP	65/120 (55)	3.5	<p>Hybrid Heat Pump</p>  <p>(Jensen et al., 2015a, 2015b)</p>	 <table border="1" data-bbox="1612 506 1908 596"> <thead> <tr> <th>T_{LT}/T_{HT} (ΔT_{Lift})</th> <th>COP</th> </tr> </thead> <tbody> <tr> <td>20/95 (75)</td> <td>2.4</td> </tr> <tr> <td>40/100 (60)</td> <td>4.5</td> </tr> </tbody> </table>	T_{LT}/T_{HT} (ΔT_{Lift})	COP	20/95 (75)	2.4	40/100 (60)	4.5
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<p>Mayekawa transkritische CO₂ heat pump Eco Sirocco</p>  <p>(IEA, 2014a; Mayekawa, 2010; Watanabe, 2013)</p>	 <table border="1" data-bbox="749 896 1058 986"> <thead> <tr> <th>T_{LT}/T_{HT} (ΔT_{Lift})</th> <th>COP</th> </tr> </thead> <tbody> <tr> <td>20/100 Luft (80)</td> <td>3.4</td> </tr> <tr> <td>25/120 H₂O (95)</td> <td>2.9</td> </tr> </tbody> </table>	T_{LT}/T_{HT} (ΔT_{Lift})	COP	20/100 Luft (80)	3.4	25/120 H ₂ O (95)	2.9	<p>Thermeco₂ HHR1000 with 6 piston compressors, up to 1100 kW</p>  <p>(Dürr thermea GmbH, 2016; IEA, 2014a; Thermea, 2012)</p>	 <table border="1" data-bbox="1612 929 1934 991"> <thead> <tr> <th>T_{LT}/T_{HT} (ΔT_{Lift})</th> <th>COP</th> </tr> </thead> <tbody> <tr> <td>20/80 (60)</td> <td>3.9-4.3</td> </tr> </tbody> </table>	T_{LT}/T_{HT} (ΔT_{Lift})	COP	20/80 (60)	3.9-4.3
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<p>Ochsner IWHS 400 ER3 screw compressor, 380 kW</p>  <p>(Ochsner, 2015)</p>	 <table border="1" data-bbox="762 1282 1058 1343"> <thead> <tr> <th>T_{LT}/T_{HT} (ΔT_{Lift})</th> <th>COP</th> </tr> </thead> <tbody> <tr> <td>45/90 (45)</td> <td>4.0</td> </tr> </tbody> </table>	T_{LT}/T_{HT} (ΔT_{Lift})	COP	45/90 (45)	4.0	<p>Ochsner IWDS 330 ER3 screw compressor, 312 kW</p>  <p>(Zauner, 2016)</p>	 <table border="1" data-bbox="1612 1286 1908 1348"> <thead> <tr> <th>T_{LT}/T_{HT} (ΔT_{Lift})</th> <th>COP</th> </tr> </thead> <tbody> <tr> <td>50/105 (55)</td> <td>2.68</td> </tr> </tbody> </table>	T_{LT}/T_{HT} (ΔT_{Lift})	COP	50/105 (55)	2.68		
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Commercial HTHPs – cycles, COPs and pictures

<p>Combitherm</p>  <p>(Blesl et al., 2014; Wolf et al., 2014)</p>	 <table border="1"> <thead> <tr> <th>$T_{LT}/T_{HT} (\Delta T_{Lift})$</th> <th>COP</th> </tr> </thead> <tbody> <tr> <td>50/100 (50)</td> <td>3.1-3.4</td> </tr> </tbody> </table>	$T_{LT}/T_{HT} (\Delta T_{Lift})$	COP	50/100 (50)	3.1-3.4	<p>Friotherm Unitop 22/22 3'300 kW, 2-stage turbo</p>  <p>(Friotherm AG, 2005; Wojtan, 2016)</p>	 <table border="1"> <thead> <tr> <th>$T_{LT}/T_{HT} (\Delta T_{Lift})$</th> <th>COP</th> </tr> </thead> <tbody> <tr> <td>34/95 (61)</td> <td>3.51</td> </tr> </tbody> </table>	$T_{LT}/T_{HT} (\Delta T_{Lift})$	COP	34/95 (61)	3.51				
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<p>Star Refrigeration Neatpump NP601 380 kW to 2.6 MW, Vilter VSSH screw 76 bar</p>  <p>(EMERSON, 2012)</p>	 <table border="1"> <thead> <tr> <th>$T_{LT}/T_{HT} (\Delta T_{Lift})$</th> <th>COP</th> </tr> </thead> <tbody> <tr> <td>50/90 (40)</td> <td>3-4</td> </tr> <tr> <td>35/80 (45)</td> <td>5</td> </tr> <tr> <td>39/90 (51)</td> <td>4</td> </tr> </tbody> </table>	$T_{LT}/T_{HT} (\Delta T_{Lift})$	COP	50/90 (40)	3-4	35/80 (45)	5	39/90 (51)	4	<p>GEA Grasso FX P Heat Pump Double screw 63 bar</p>  <p>(Dietrich and Fredrich, 2012)</p>	 <table border="1"> <thead> <tr> <th>$T_{LT}/T_{HT} (\Delta T_{Lift})$</th> <th>COP</th> </tr> </thead> <tbody> <tr> <td>35/80 (45)</td> <td>5.0</td> </tr> </tbody> </table>	$T_{LT}/T_{HT} (\Delta T_{Lift})$	COP	35/80 (45)	5.0
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<p>Johnson Controls SABROE HeatPAC™-HPX piston compressor 60 bar</p>  <p>(Johnson Controls, 2017)</p>	 <table border="1"> <thead> <tr> <th>$T_{LT}/T_{HT} (\Delta T_{Lift})$</th> <th>COP</th> </tr> </thead> <tbody> <tr> <td>39/90 (51)</td> <td>4.0</td> </tr> </tbody> </table>	$T_{LT}/T_{HT} (\Delta T_{Lift})$	COP	39/90 (51)	4.0	<p>Kobelco HEM-HR90 double screw (2-stage)</p>  <p>(Kuromaki, 2012; Oue and Okada, 2013)</p>	 <table border="1"> <thead> <tr> <th>$T_{LT}/T_{HT} (\Delta T_{Lift})$</th> <th>COP</th> </tr> </thead> <tbody> <tr> <td>17/90 (73)</td> <td>4.5</td> </tr> <tr> <td>35/90 (55)</td> <td>5.8</td> </tr> </tbody> </table>	$T_{LT}/T_{HT} (\Delta T_{Lift})$	COP	17/90 (73)	4.5	35/90 (55)	5.8		
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<p>Viessmann Vitocal 350-HT Pro</p>  <p>(Viessmann, 2016)</p>	 <table border="1"> <thead> <tr> <th>$T_{LT}/T_{HT} (\Delta T_{Lift})$</th> <th>COP</th> </tr> </thead> <tbody> <tr> <td>50/90 (40)</td> <td>3.4</td> </tr> </tbody> </table>	$T_{LT}/T_{HT} (\Delta T_{Lift})$	COP	50/90 (40)	3.4	<p>Mitsubishi ETW-L</p>  <p>(IEA, 2014a; Watanabe, 2013).</p>	 <table border="1"> <thead> <tr> <th>$T_{LT}/T_{HT} (\Delta T_{Lift})$</th> <th>COP</th> </tr> </thead> <tbody> <tr> <td>50/90 (40)</td> <td>4.1</td> </tr> </tbody> </table>	$T_{LT}/T_{HT} (\Delta T_{Lift})$	COP	50/90 (40)	4.1				
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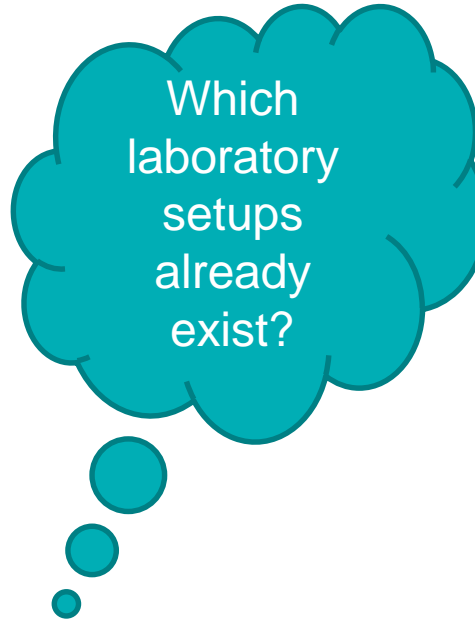
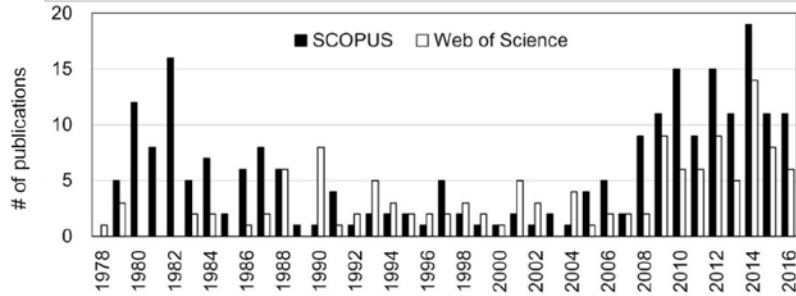
COP vs. temperature lift for various commercial HTHPs



- Average values: $COP = 3.2 \pm 0.9$
 $\Delta T_{Lift} = 66 \pm 24 K$
- Most data points between 40 to 60% Carnot efficiency (at 140°C supply temperature)

Research status on HTHPs

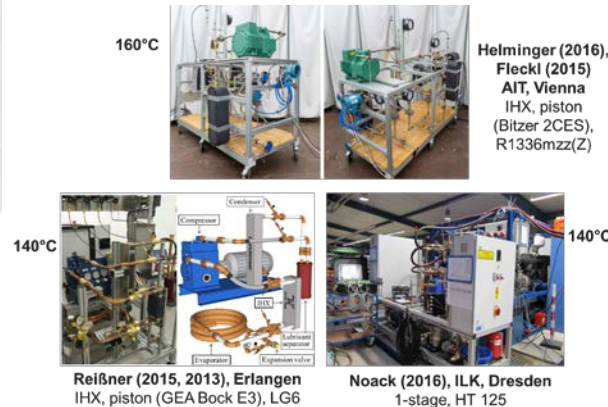
Publications



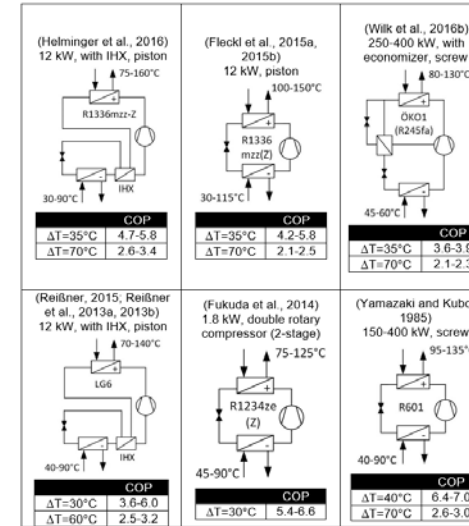
Research projects

Organisation, Project partners	Cycle	Compressor type	Refrigerant	Source and supply temperatures [°C]							Heating capacity [kW]	Reference
				20	40	60	80	100	120	140		
Austrian Institute of Technology (AIT), Wien, Chemours, Bitzer	IHX	piston	R1336mzz-Z								12	(Helming et al., 2016)
Austrian Institute of Technology (AIT), Wien, Chemours, Bitzer	1-stage	piston	R1336mzz-Z								12	(Fleckl et al., 2015a, 2015b)
PACO, University Lyon, EDF Electricité de France	fish tank	double screw	H ₂ O (Vivasse)								300	(Chamoun et al., 2014, 2013, 2012a, 2012b)
Institut für Luft- und Kältetechnik (ILK), Dresden	1-stage	n.a.	HT 125								12	(Noack, 2016)
Friedrich-Alexander Universität Erlangen-Nürnberg, Siemens	IHX	piston	LG6								10	(Reißner, 2015; Reißner et al., 2013a, 2013b)
Alter ECO, EDF Electricité de France	IHX and subcooler	double scroll	ECO3 (R245fa)								50-200	(Bobelin et al., 2012; IEA, 2014a)
Tokyo Electric Power Company, Japan	1-stage	screw	R601								150-400	(Yamazaki and Kubo, 1985)
Austrian Institute of Technology (AIT), Wien, Edlmayer, Ochsner	economizer	screw	ÖKO1 (R245fa)								250-400	(Wilk et al., 2016b)
Kyushu University, Fukuoka, Japan	1-stage	double rotary (2-stage)	R1234ze(Z)								1.8	(Fukuda et al., 2014)
Johnson Controls, EDF Electricité de France	economizer and IHX	double screw centrifugal turbo	R245fa								300-500 900-1200	(IEA, 2014a)

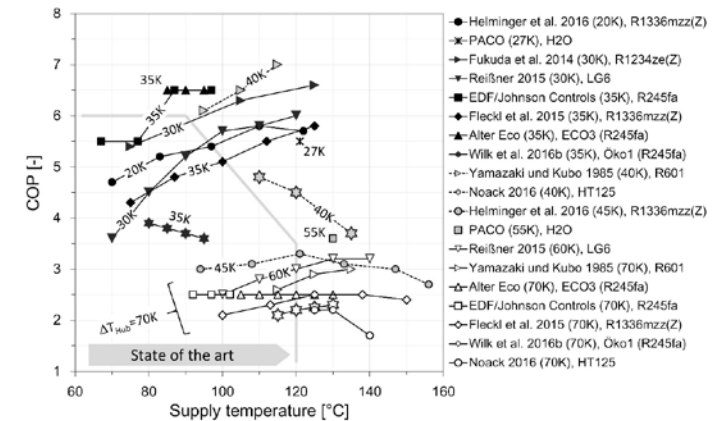
Experimental setups



Cycles

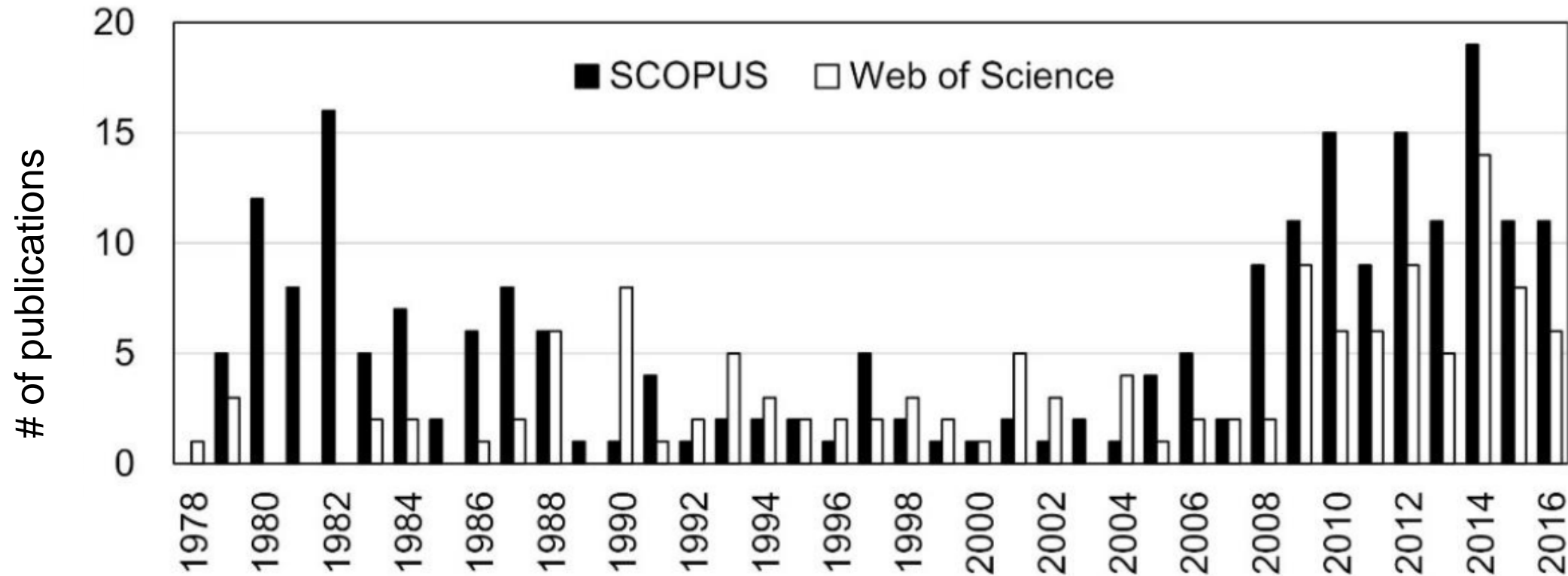


COP vs. supply temperature



Research activity on HTHPs

Number of publications



Number of publications with search key word «high temperature heat pump» in databases SCOPUS (www.scopus.com) and Web of Science (www.webofknowledge.com)

Research projects in the field of HTHPs

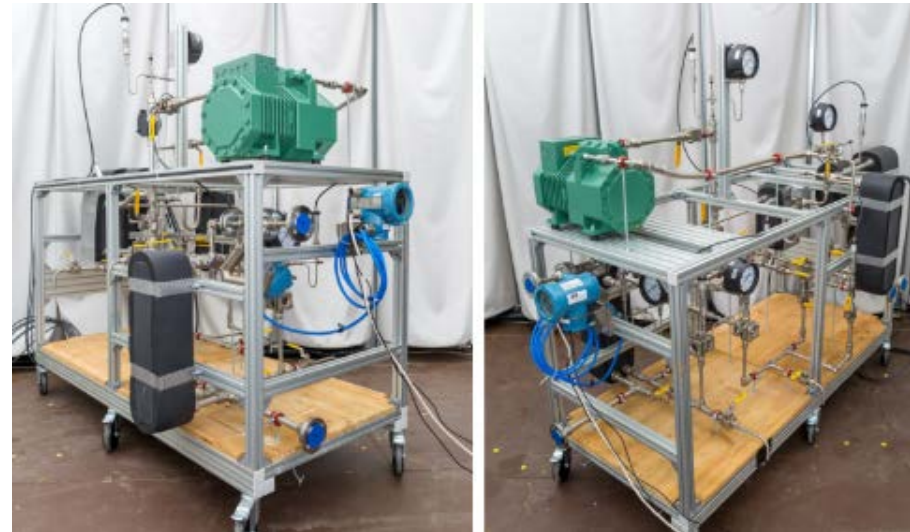
with information on the organization, project partners, heat pump cycle, compressor type, refrigerant, heating capacity and sorted by the sink temperature

Organisation, Project partners	Cycle	Compressor type	Refrigerant	Source and supply temperatures [°C]							Heating capacity [kW]	Reference		
				20	40	60	80	100	120	140			160	
Austrian Institute of Technology (AIT), Wien, Chemours, Bitzer	IHX	piston	R1336mzz-Z										12	(Helminger et al., 2016)
Austrian Institute of Technology (AIT), Wien, Chemours, Bitzer	1-stage	piston	R1336mzz-Z										12	(Fleckl et al., 2015a, 2015b)
PACO, University Lyon, EDF Electricité de France	flash tank	double screw	H ₂ O (Wasser)										300	(Chamoun et al., 2014, 2013, 2012a, 2012b)
Institut für Luft- und Kältetechnik (ILK), Dresden	1-stage	n.a.	HT 125										12	(Noack, 2016)
Friedrich-Alexander Universität Erlangen-Nürnberg, Siemens	IHX	piston	LG6										10	(Reißner, 2015; Reißner et al., 2013a, 2013b)
Alter ECO, EDF Electricité de France	IHX and subcooler	double scroll	ECO3 (R245fa)										50-200	(Bobelin et al., 2012; IEA, 2014a)
Tokyo Electric Power Company, Japan	1-stage	screw	R601										150-400	(Yamazaki and Kubo, 1985)
Austrian Institute of Technology (AIT), Wien, Edtmayer, Ochsner	economizer	screw	ÖKO1 (R245fa)										250-400	(Wilk et al., 2016b)
Kyushu University, Fukuoka, Japan	1-stage	double rotary (2-stage)	R1234ze(Z)										1.8	(Fukuda et al., 2014)
Johnson Controls, EDF Electricité de France	economizer and IHX	double screw centrifugal turbo	R245fa										300-500 900-1'200	(IEA, 2014a)

Experimental setups

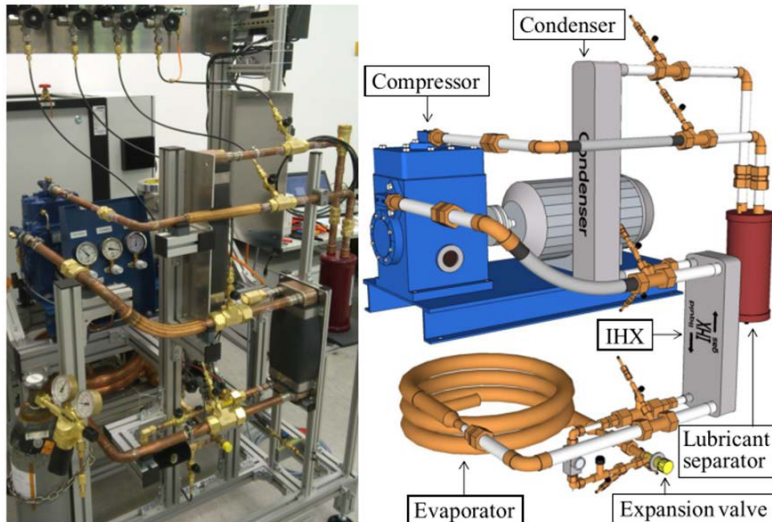
HTHPs in research status

160°C



**Helminger (2016),
Fleckl (2015)**
AIT, Vienna
1-stage cycle with
IHX, piston
(Bitzer 2CES),
R1336mzz(Z)

140°C



Reißner (2015, 2013), Erlangen
1-stage with IHX, piston (GEA Bock E3), LG6

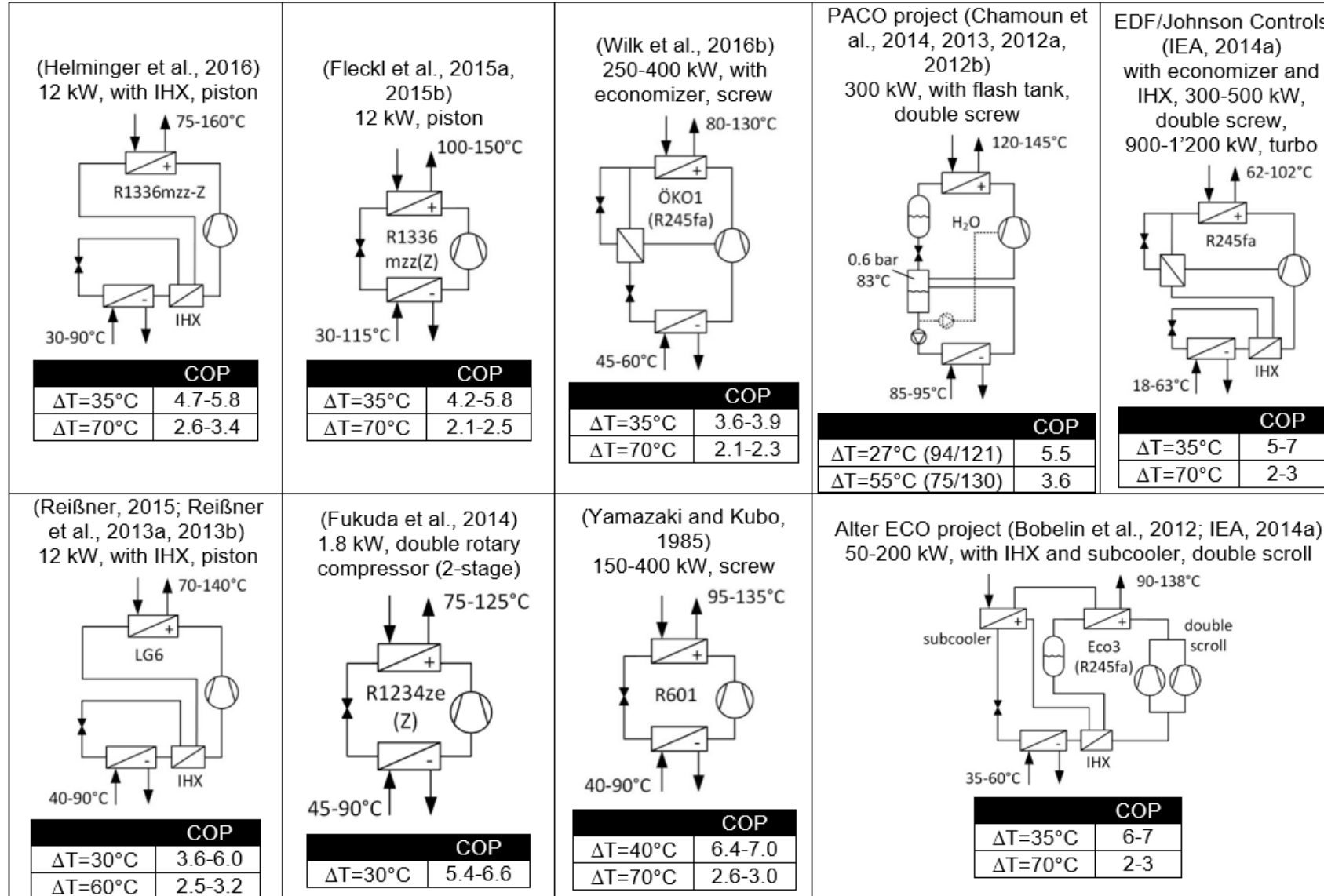
140°C



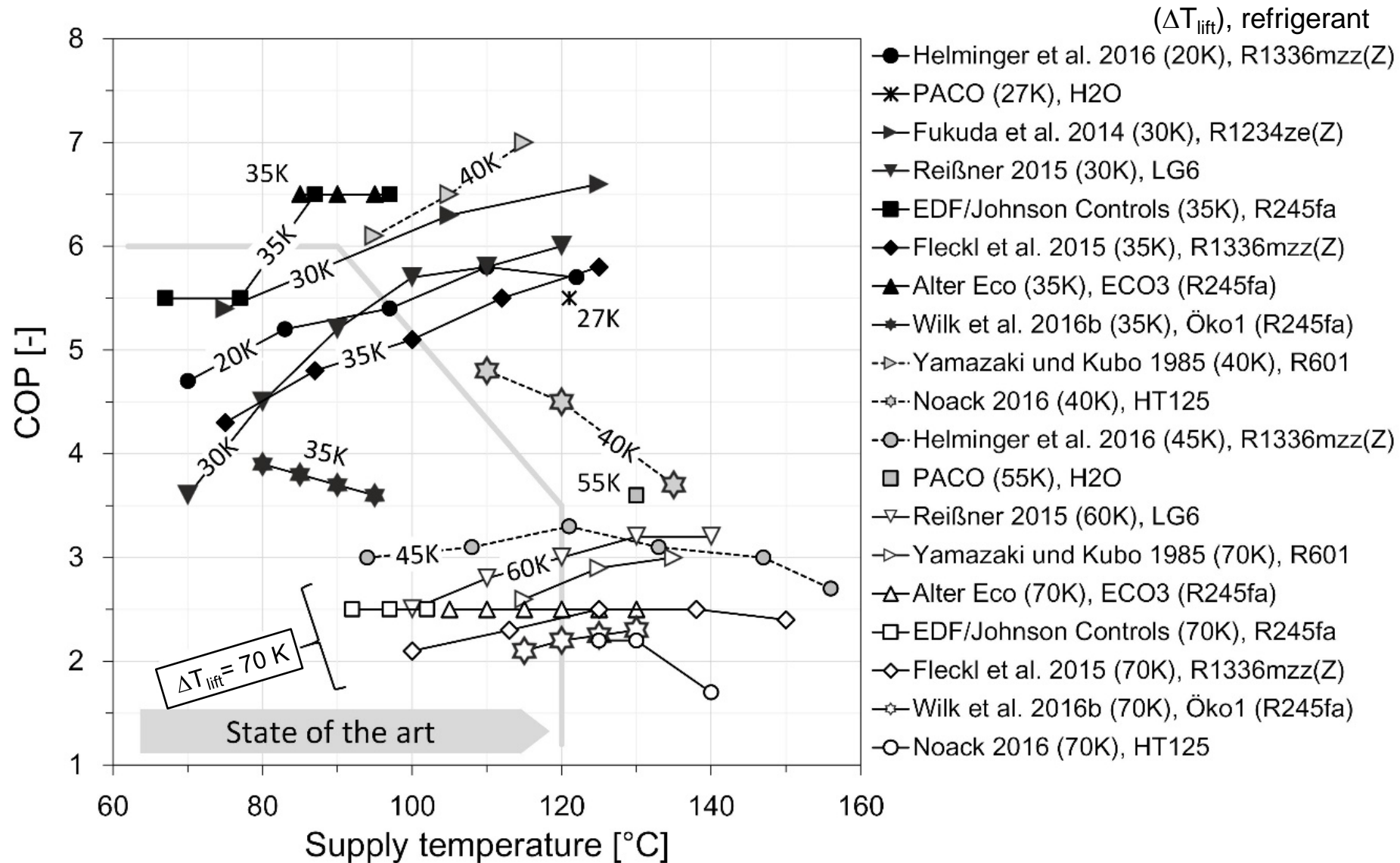
Noack (2016), ILK, Dresden
1-stage cycle, HT 125

Cycles and achieved COPs

HTHPs in research status



Achieved COPs of HTHPs in research status versus supply temperature at constant temperature lifts (ΔT_{lift}) of 20 to 70 K

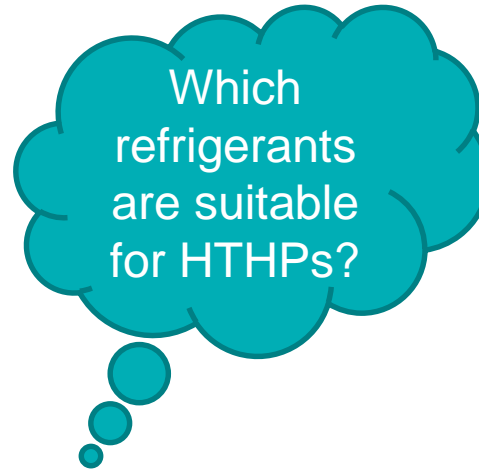


State of the art indicated at 120°C supply temperature and a COP of up to 6 at 60 to 90°C.

Refrigerants for HTHPs

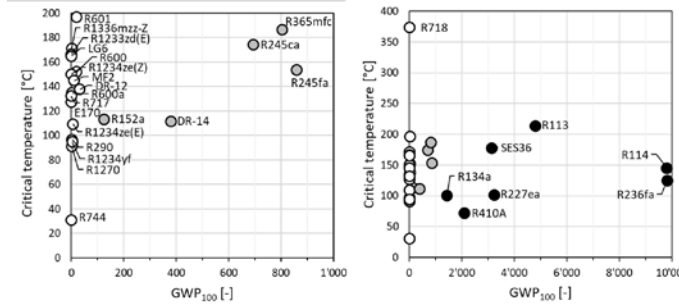
Selection criteria

Criteria	Required properties
Thermal suitability	High critical temperature, low critical pressure
Environmental	ODP = 0, low GWP, short atmospheric life
Safety	Non-toxic, non-combustible (safety group A1)
Efficiency	High COP, low pressure ratio, minimal overheat to prevent fluid compression, high volumetric capacity
Availability	Available on the market, low price
Other factors	Good solubility in oil, thermal stability of the refrigerant-oil mixture, lubricating properties at high temperatures, material compatibility with steel and copper



Critical temperature vs. GWP

○ GWP < 20 ● 20 < GWP < 1'000 ● GWP > 1'000



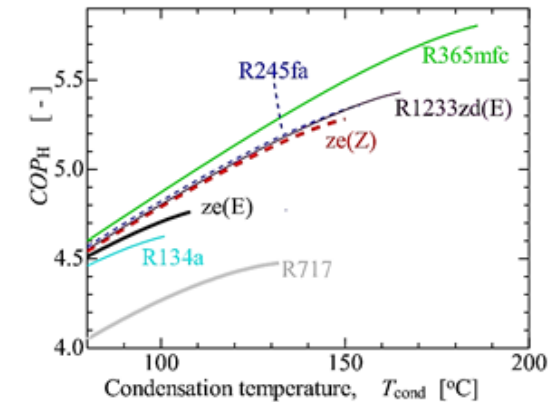
Price

Refrigerant	CAS Nr.	Container [kg]	Price per kg [Euro]	Factor to R134a
R134a	811-97-2	12	8.55	1.0
		28	8.55	1.0
		63	8.25	1.0
R410A	75-10-5 (50%) 354-33-6 (50%)	10	8.85	1.0
		22	8.85	1.0
		53	8.60	1.0
R744	124-38-9	30	9.00	1.1
R1234ze(E)	1645-83-6	11	49.50	5.8
		59	69.90	8.2
R1233zd		14	48.25	5.6
R1233zd		14	62.70	7.3
R245fa	460-73-1	14	63.65	7.4
			87.90	10.3
R1234yf	754-12-1	5	163.35	19.1
			229.60	26.9

Refrigerant properties

Refrigerant	Description	Chemical formula	T _{crit} [°C]	P _{crit} [bar]	ODP [-]	GWP ₁₀₀ [-]	SG	Bp. [°C]	M [g/mol]
Ethane line									
R113	1,1,2-Trichloro-1,2,2-trifluoroethane	CCl ₂ FCClF ₂	214.0	33.9	0.8	4900	A1	47.6	187.4
R114	1,2-Dichloro-1,1,2,2-tetrafluoroethane	CClF ₂ CClF ₂	145.7	32.6	1	9900	A1	3.8	170.9
R134a	1,1,1,2-Tetrafluoroethane	CH ₂ FCF ₃	101.1	40.6	0	1430	A1	-26.1	102.0
R152a	1,1-Difluoroethane	CH ₃ CHF ₂	113.3	45.2	0	124	A2	-24.0	66.1
Propane line									
R245ca	1,1,2,2,3-Pentafluoropropane	CHF ₂ CF ₂ CHF	174.4	39.3	0	693	n.v.	25.1	134.0
R245fa	1,1,2,2,3-Pentafluoropropane	CHF ₂ CF ₂ CF ₃	154.0	36.5	0	858	B1	14.9	134.0
R236fa	1,1,1,3,3,3-Hexafluoropropane	CF ₃ CF ₂ CF ₃	124.9	32.0	0	9810	A1	-1.4	152.0
R227ea	1,1,1,2,3,3,3-Heptafluoropropane	CF ₃ CF ₂ CF ₃	101.8	29.3	0	3220	A1	-15.6	170.0
R290	Propane	CH ₃ CH ₂ CH ₃	96.7	42.5	0	3	A3	-42.1	44.1
R1270	Propene	CH ₃ CH=CH ₂	91.1	45.6	0	2	A3	-47.6	42.1
Butane line									
R365mfc	1,1,1,3,3-Pentafluorobutane	CF ₃ CH ₂ CF ₂ CF ₃	186.9	32.7	0	604	A2	40.2	148.1
SE536	Pentafluorobutane	R365mfc/PPFE65/35	177.6	28.5	0	3'126	A2	35.6	184.5
Hydrocarbons									
R601	Pentane	CH ₃ CH ₂ CH ₂ CH ₂ CH ₃	196.6	33.7	0	20	A3	36.1	72.2
R600	Butane	CH ₃ CH ₂ CH ₂ CH ₃	152.0	38.0	0	20	A3	-0.5	58.1
R600a	Isobutane	CH(CH ₃) ₂ CH ₃	134.7	36.3	0	3	A3	-11.8	58.1
Refrigerant mixtures									
R410A	R32/R125 (50/50)	CH ₂ F ₂ /CHF ₂ CF ₃	72.6	49.0	0	2088	A1	-51.5	72.6
Hydro Fluoro Olefines (HFOs)									
R1336mzz-Z	1,1,1,4,4,4-Hexafluoro-2-butene	CF ₃ CH=CHCF ₂ (Z)	171.3	29.0	0	2	A1	33.4	164.1
R1233zd(E)	Tetrafluoropropene	CF ₃ CH=CHCl(trans)	166.5	36.2	0.0003	1	A1	18.0	130.5
R1234ze(Z)	cis-1,3,3,3-Tetrafluoro-1-propene	CF ₃ CH=CHF(cis)	150.1	35.3	0	1	A2	9.8	114.0
R1234ze(E)	trans-1,3,3,3-Tetrafluoro-1-propene	CF ₃ CH=CHF(trans)	109.4	36.4	0	7	A2L	-19.0	114.0
R1234yf	2,3,3,3-Tetrafluoro-1-propene	CF ₃ CF=CH ₂	94.7	33.8	0	4	A2L	-29.5	114.0
DR-14	n.a.	n.a.	111.6	39.6	0	390	A1	-20.5	n.v.
DR-12	n.a.	n.a.	137.7	30.0	0	32	1	7.5	n.v.
LG6	n.a.	n.a.	165.0	n.a.	0	1	n.a.	n.a.	n.a.
MF2	n.a.	n.a.	145.0	n.a.	0	10	n.a.	n.a.	n.a.
Others									
E170	Dimethyl ether	CH ₃ OCH ₃	127.2	53.4	0	1	A3	-24.8	46.1
R718	Water	H ₂ O	373.9	220.6	0	0	A1	100.0	18.0
R717	Ammonia	NH ₃	132.3	113.3	0	0	B2L	-33.3	17.0
R744	Carbon dioxide	CO ₂	31.0	73.8	0	1	A1	-78.5	44.0

Efficiency



Safety

Flammability	higher	A3	R290, R1270, R601, R600, R600a, E170	B3	
no flame propagation	A1		R113, R114, R134a, R236fa, R227ea, R410A, R1336mzz-Z, R1233zd(E), DR-14, DR-12, R718, R744	B1	R245ca, R245fa
			lower	higher	
Toxicity					

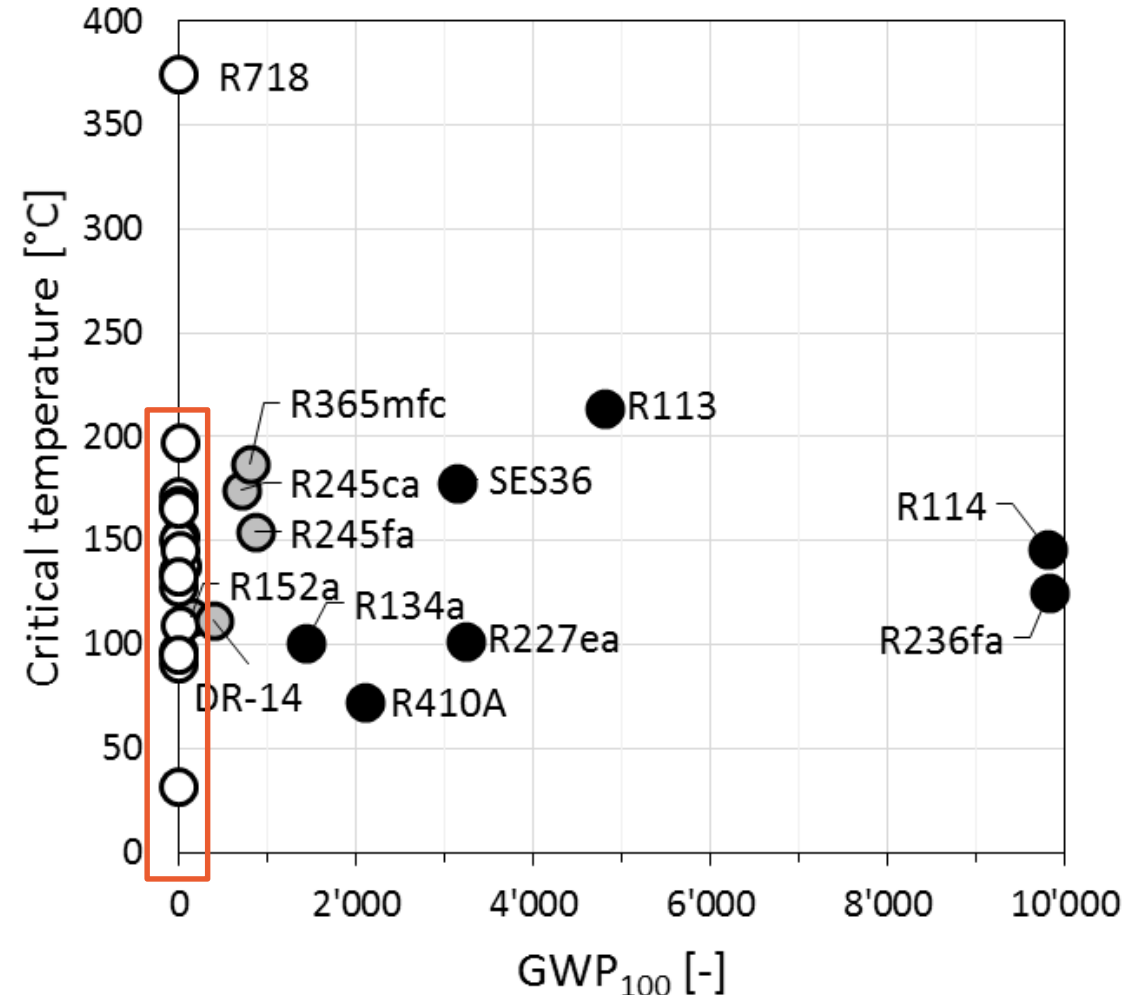
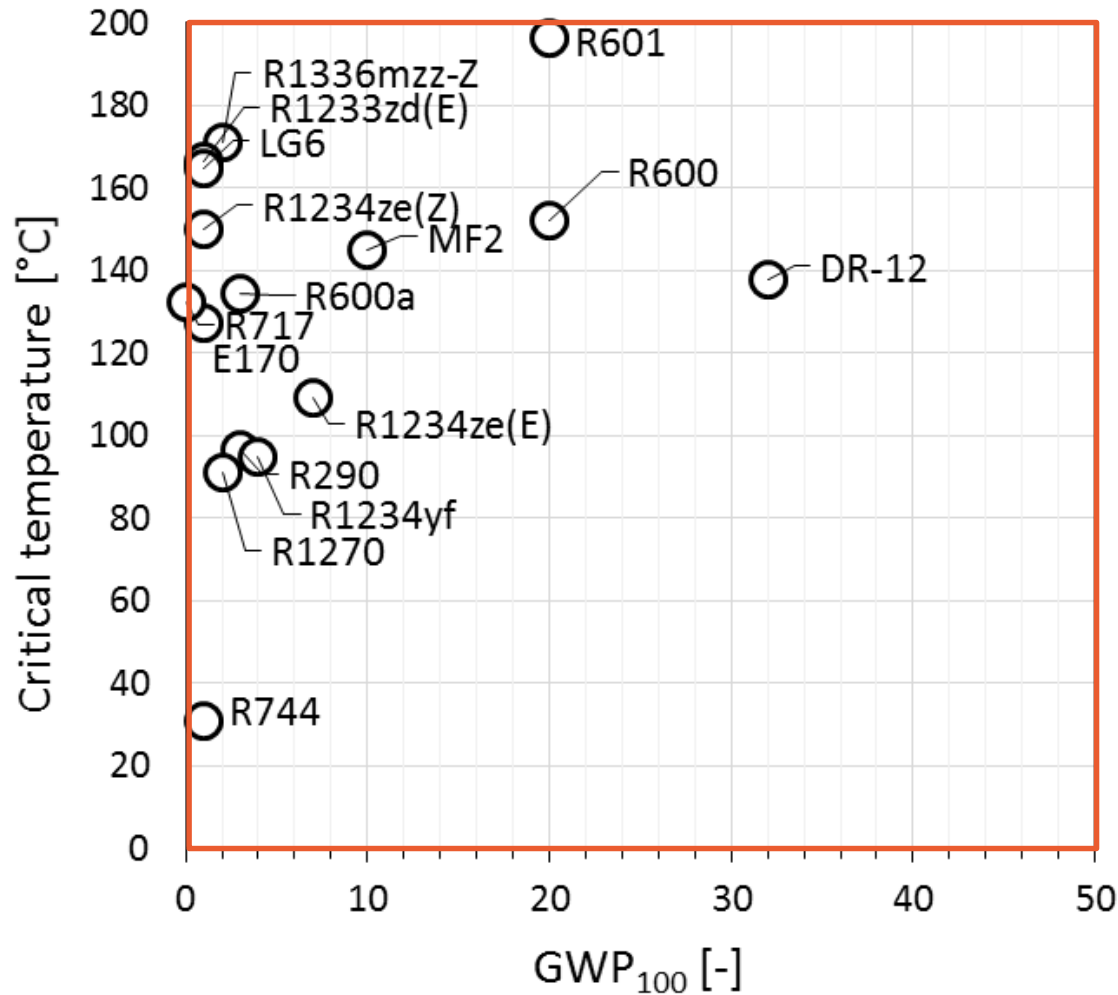
Selection criteria for refrigerants for HTHPs

Criteria	Required properties
Thermal suitability	High critical temperature, low critical pressure
Environmental	ODP = 0, low GWP, short atmospheric life
Safety	Non-toxic, non-combustible (safety group A1)
Efficiency	High COP, low pressure ratio, minimal overheat to prevent fluid compression, high volumetric capacity
Availability	Available on the market, low price
Other factors	Good solubility in oil, thermal stability of the refrigerant-oil mixture, lubricating properties at high temperatures, material compatibility with steel and copper

Data sources: Bertinat (1986), Burtscher et al. (2009), Calm (2008), Eisa et al. (1986), Göktun (1995), Helminger et al. (2016), Klein (2009), Kujak (2016), Reißner et al. (2013), Rieberer et al. (2015)

Classification of refrigerants by critical temperature and GWP

○ GWP < 50 ◐ 50 < GWP < 1'000 ● GWP > 1'000



Safety Group Classification

according to DIN EN 378-1 (2008) and ASHRAE 34

Flammability	higher	A3	R290, R1270, R601, R600, R600a, E170	B3	
	lower	A2	R152a, R365mfc, SES36, R1234ze(Z), R1234ze(E), R1234yf	B2	R717
	no flame propagation	A1	R113, R114, R134a, R236fa, R227ea, R410A, R1336mzz(Z), R1233zd(E), DR-14, DR-12, R718, R744	B1	R245ca, R245fa
		lower		higher	
Toxicity					

Properties of refrigerants for HTHPs

Refrigerant	Description	Chemical formula	T _{crit} [°C]	p _{crit} [bar]	ODP [-]	GWP ₁₀₀ [-]	SG	Bp. [°C]	M [g/mol]
Ethane line									
R113	1,1,2-Trichloro-1,2,2-trifluoroethane	CCl ₂ FCClF ₂	214.0	33.9	0.8	4'800	A1	47.6	187.4
R114	1,2-Dichloro-1,1,2,2-tetrafluoroethane	CClF ₂ CClF ₂	145.7	32.6	1	9'800	A1	3.8	170.9
R134a	1,1,1,2-Tetrafluoroethane	CH ₂ FCF ₃	101.1	40.6	0	1'430	A1	-26.1	102.0
R152a	1,1-Difluoroethane	CH ₃ CHF ₂	113.3	45.2	0	124	A2	-24.0	66.1
Propane line									
R245ca	1,1,2,2,3-Pentafluoropropane	CHF ₂ CF ₂ CH ₂ F	174.4	39.3	0	693	n.v.	25.1	134.0
R245fa	1,1,2,2,3-Pentafluoropropane	CHF ₂ CH ₂ CF ₃	154.0	36.5	0	858	B1	14.9	134.0
R236fa	1,1,1,3,3,3-Hexafluoropropane	CF ₃ CH ₂ CF ₃	124.9	32.0	0	9'810	A1	-1.4	152.0
R227ea	1,1,1,2,3,3,3-Heptafluoropropane	CF ₃ CHFCF ₃	101.8	29.3	0	3'220	A1	-15.6	170.0
R290	Propane	CH ₃ CH ₂ CH ₃	96.7	42.5	0	3	A3	-42.1	44.1
R1270	Propene	CH ₃ CH=CH ₂	91.1	45.6	0	2	A3	-47.6	42.1
Butane line									
R365mfc	1,1,1,3,3-Pentafluorobutane	CF ₃ CH ₂ CF ₂ CH ₃	186.9	32.7	0	804	A2	40.2	148.1
SES36	Pentafluorobutane	R365mfc/PFPE65/35	177.6	28.5	0	3'126	A2	35.6	184.5
Hydrocarbons									
R601	Pentane	CH ₃ CH ₂ CH ₂ CH ₂ CH ₃	196.6	33.7	0	20	A3	36.1	72.2
R600	Butane	CH ₃ CH ₂ CH ₂ CH ₃	152.0	38.0	0	20	A3	-0.5	58.1
R600a	Isobutane	CH ₃ (CH ₃) ₂ CH ₃	134.7	36.3	0	3	A3	-11.8	58.1
Refrigerant mixtures									
R410A	R32/R125 (50/50)	CH ₂ F ₂ /CHF ₂ CF ₃	72.6	49.0	0	2'088	A1	-51.5	72.6
Hydro Fluoro Olefines (HFOs)									
R1336mzz-Z	1,1,1,4,4,4-Hexafluoro-2-butene	CF ₃ CH=CHCF ₃ (Z)	171.3	29.0	0	2	A1	33.4	164.1
R1233zd(E)	Tetrafluorpropene	CF ₃ CH=CHCl(trans)	166.5	36.2	0.0003	1	A1	18.0	130.5
R1234ze(Z)	cis-1,3,3,3-Tetrafluoro-1-propene	CF ₃ CH=CHF(cis)	150.1	35.3	0	1	A2	9.8	114.0
R1234ze(E)	trans-1,3,3,3-Tetrafluoro-1-propene	CF ₃ CH=CHF(trans)	109.4	36.4	0	7	A2L	-19.0	114.0
R1234yf	2,3,3,3-Tetrafluoro-1-propene	CF ₃ CF=CH ₂	94.7	33.8	0	4	A2L	-29.5	114.0
DR-14	n.a.	n.a.	111.6	39.6	0	380	A1	-20.5	n.v.
DR-12	n.a.	n.a.	137.7	30.0	0	32	1	7.5	n.v.
LG6	n.a.	n.a.	165.0	n.a.	0	1	n.a.	n.a.	n.a.
MF2	n.a.	n.a.	145.0	n.a.	0	10	n.a.	n.a.	n.a.
Others									
E170	Dimethyl ether	CH ₃ OCH ₃	127.2	53.4	0	1	A3	-24.8	46.1
R718	Water	H ₂ O	373.9	220.6	0	0	A1	100.0	18.0
R717	Ammonia	NH ₃	132.3	113.3	0	0	B2L	-33.3	17.0
R744	Carbon dioxide	CO ₂	31.0	73.8	0	1	A1	-78.5	44.0

T_{crit} = critical temperature

p_{crit} = critical pressure

ODP = Ozone Depletion Potential (R11=1.0)

GWP = Global Warming Potential (CO₂=1.0, 100 years EU F-Gas regulation 517/2014)

SG = Safety group (according to DIN EN 378-1, 2008, ASHRAE 34)

Bp. = Boiling point at 1.013 bar

M = Molecular weight

 excluded

 suitable

Conclusions

Market overview

- **More than 20 HTHP models** identified with supply temperatures > 90°C from 13 manufacturers (e.g. Vicking HeatBooster with 150°C, Ochsner IWWDS with 130°C, Kobelco SGH120, Mayekawa Eco Sirocco, and Hybrid Energy Heat Pump with 120°C)
- **Heat source:** water, brine, waste heat (17 to 65°C)
- **COP:** 2.4 to 5.8 at a temperature lift of 40 to 95 K
- **Heating capacity:** from about 20 kW to 20 MW
- **Refrigerants:** R245fa, R717 (NH₃), R744 (CO₂), R134a, R1234ze(E)
- **Compressors:** 1- and 2-shaft screws, 2-stage turbos, pistons (parallel)
- **Cycles:** usually 1-stage, optimization by IHX, parallel compressors, economizer, intermediate injection, 2-stage cascade (R134a/R245fa) or with a flash economizer

Research status

- **Highest supply temperature of 160°C** at AIT (Vienna), 1-stage cycle with IHX and R1336mzz(Z)
- **At least 10 research projects** reached > 100°C
- **Heating capacity:** lab scale 12 kW, larger prototypes >100 kW
- **COPs** (at 120°C supply temperature): 5.7 to 6.5 (30 K temperature lift), 2.2 to 2.8 (70 K)
- **Cycles all 1-stage:** partly with IHX and/or economizer with intermediate injection
- **Refrigerants:** R1336mzz(Z), R718 (H₂O), R245fa, R1234ze (Z), R601, LG6 (Siemens), ÖKO1 (contains R245fa, Ochsner), ECO3 (R245fa, Alter ECO), HT125 (ILK, Dresden)
- **Compressors:** pistons in lab systems
- **HFO refrigerants:** thermodynamic suitable, good efficiency, GWP <10, ODP = 0, safe, future-proof according to F-Gas regulation

Thank you for your attention

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